

Research paper**Adsorption of 2,4-D on carbonized chest nut shell****Abstract**

The adsorption of 2,4-D in 4×10^{-4} g/l aqueous solution on carbonized chest nut shell (CCS) was studied at 25 °C temperature. The adsorption data was modelled by using Langmuir and Freundlich isotherms. The adsorption data fit well with Freundlich isotherm that indicates the pesticide adsorption is heterogeneous type and multi layer characteristics. The effect of pH on adsorption was also studied. The adsorption capacity is quite high in acidic medium (pH=3). The carbonized chestnut shell was a good and cheap adsorbent which can be utilized in the place of active carbon.

Introduction

Pollution of surface and ground waters causes risk to human health in the case of the potential health hazards of their constituents of anorganic and organic compounds. Pesticides are like hazardous compounds that cause water pollution due to their extensive application for rodenticides, insecticides, acaricides, repellants, fungicides, algicides, herbicides, etc. The common usage of these chemicals has some undesirable effects such as toxicity, carcinogenicity and mutagenicity [1, 2, 3]. Among the numerous agrochemicals, the herbicide 2,4-D has been applied to control plants in gardens and in agriculture. It is used for low cost and good selectivity. The maximum allowable concentration must be under 100 ppb in drinking water due to toxic effect and poorly biodegradable characteristics. It is extremely difficult for applying a single method for pesticide disposal due to wide range usage. Adsorption on solid substances such as soils, clays, microorganisms or activated carbon can be used for removing pesticides from waters [4-10].

Adsorption process is efficient for the removal of colors, odors, organic and biologic materials from process. Activated carbons are the most widely used adsorbents from the point of their

excellent adsorption abilities [11]. The high adsorption capacities of activated carbons are mostly related to their high surface area, pore volume and porosity [12]. The activation method and the nature of source materials play the important role for removing the undesired materials efficiently [13, 14].

There has been an increasing interest for removal of undesired molecules on activated carbons. This is due to the importance of discharging the pollutants from water streams and the atmosphere [15]. The adsorption process depends on several factors such as the nature of adsorbent, adsorbate and adsorption conditions. Adsorbent characteristics include the surface area, pore size distribution, ash content, hydrophobicity, the density and type of functional groups present on the surface. The nature of adsorbate depends on its polarity, its hydrophobicity, the size of the molecule and its acidity or alkalinity. The alkalinity is determined by the nature of the functional group present. Adsorption conditions include several factors such as temperature, the polarity of solvent, pH, concentrations, etc [16].

The aim of this work was to remove of 2,4-D by activated carbon made of chest nut shell with the effects of several factors such as temperature, concentration, pH, etc.

2. Materials and methods

2.1 Materials

The 2,4-D was supplied in powder form by Hektas chemical company in Turkey. The chemical formula of 2,4-D is shown in Fig 1 below. The molecular weight of 2,4-D (2,4-dichlorophenoxyacetic acid) is 221.04 g/mol. It is a solid organic substance which comes as a white powder with a melting point of 140.5 °C. Its solubility in water is 900 mg/dm³ and it is used on weeds with broad leaves. It is the most widely used herbicide in the world [17].

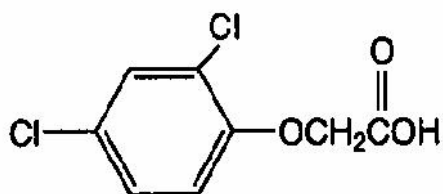
2,4-D**(2,4-dichlorophenoxy)acetic acid**

Figure 1. 2,4-D [18]

2.2 Preparation of the adsorbents

Carbonized chestnut shell (CCS) was used in the experiments. The chestnut shell was carbonized in an oven at 900 °C. 20 gr of shell were placed in the oven and carbonized under a stream of nitrogen. At the end of the heating period, the product was cooled to room temperature under nitrogen stream and the reactor was opened. Following this procedure, the carbonized material was ground and passed through 0.250 microns. Fig 2 shows the SEM graphics of CCS at the beginning (a), after carbonization stage (b) and after the experiment (c).

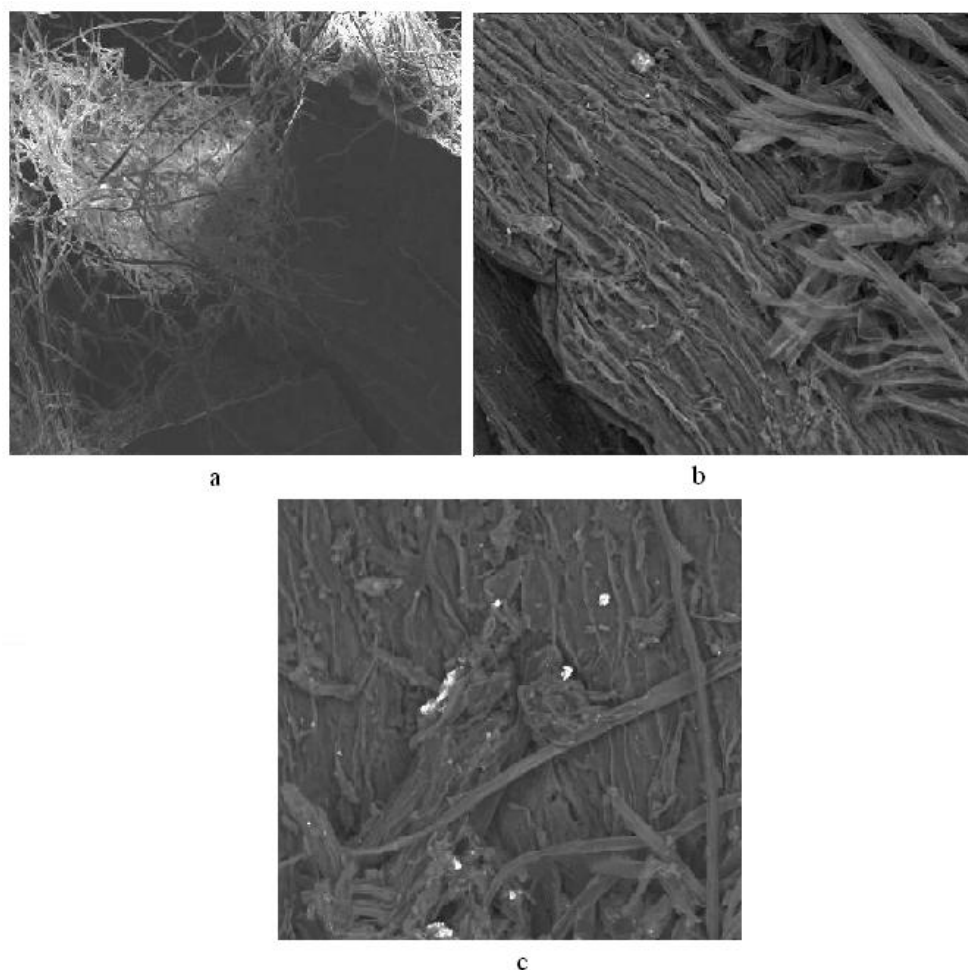


Fig 2. SEM graphics of chestnut shell a) At the beginning b) After carbonization treatment c) After experiment in 2,4-D solution) (a, 500 μm , b and c 50 μm were drawn)

2.3 Adsorption studies

A stock solution was prepared by dissolving 0.22 g 2,4-D in a liter of demineralized water as 10^{-3} g/l solution. The experimental solutions were prepared by dilution of this stock solution with deionized water to obtain concentrations of 1×10^{-4} , 2×10^{-4} , 4×10^{-4} , 6×10^{-4} 8×10^{-4} . The adsorbance-calibration data were derived from these solutions.

In the batch method, a fixed amount of adsorbent (0.1 g activated chestnut shell) was added to 100 ml solutions of 4×10^{-4} at 25 °C. The solution was stirred with a magnet for 30 minutes

following which the concentration of pesticides after equilibrium adsorption was determined spectrophotometrically at $\lambda_{\max}=280$ nm on a double beam 150-02 Shimadzu.

3. Results and discussion

3.1 Contact time and initial adsorbate concentration

The effect of initial 2,4-D concentration on adsorption on CCS was studied. Fig 3 shows the contact time of 2,4-D for 4×10^{-4} M initial concentration at 25 °C. The adsorption becomes almost constant after 250 minutes. Fig 4 shows the uptake percent of 2,4-D at 25 °C temperature.

$$\%Uptake = \frac{C_0 - C_e}{C_0} \times 100$$

C_0 = Initial concentration (mg/ml)

C_e = Equilibrium concentration (mg/ml)

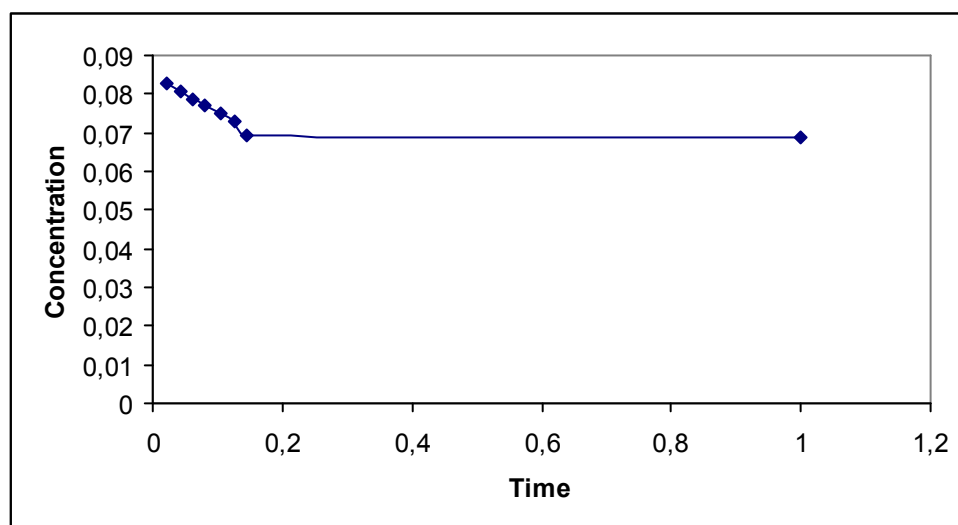


Fig 3. Equilibrium concentrations versus time at 25 °C temperature, adsorbent dose 0.1 g(100 ml)

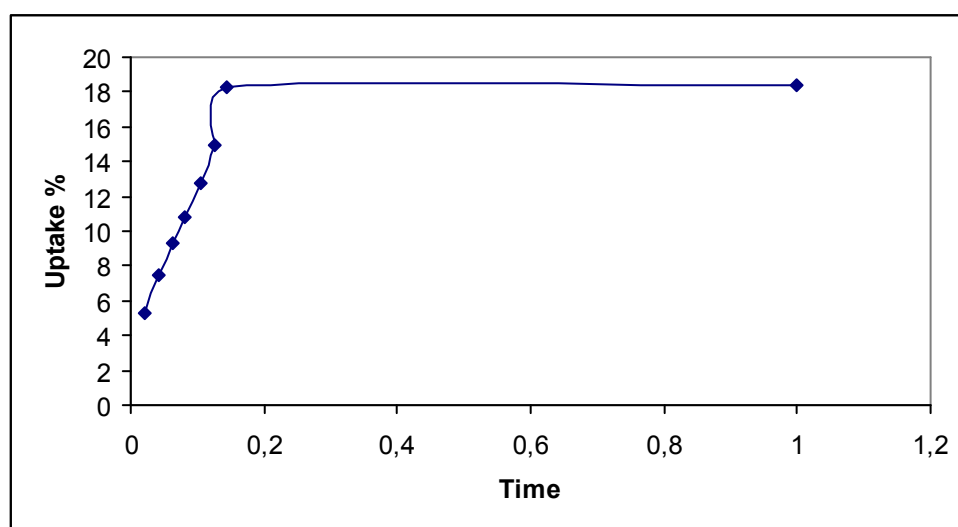


Fig 4. Uptake % versus time at 25 °C temperature, adsorbent dose 0.1 g/100 ml)

3.2 Adsorption isotherms

The equilibrium data for 2,4-D adsorption on CCS were compared by using Langmuir and Freundlich adsorption isotherms. The Langmuir isotherm model gives the uniform energies of adsorbent surfaces.

Langmuir isotherm is represented by the following equation

$$\frac{C_e}{q_e} = \frac{1}{Q_0 \cdot b} + \frac{C_e}{Q_0}$$

where C_e is the concentration of pesticide mg/l at equilibrium, q_e is the amount of adsorbate on per unit mass of adsorbent at equilibrium in mg/g, Q_0 is the maximum adsorption at monolayer coverage in mg/g, b is the adsorption equilibrium constant related to the energy of adsorption in L/mg. The plot of C_e/q_e versus C_e is linear and is presented in Fig. 5. Q_0 and b constants were found from the slope and the intercept in Fig 5.

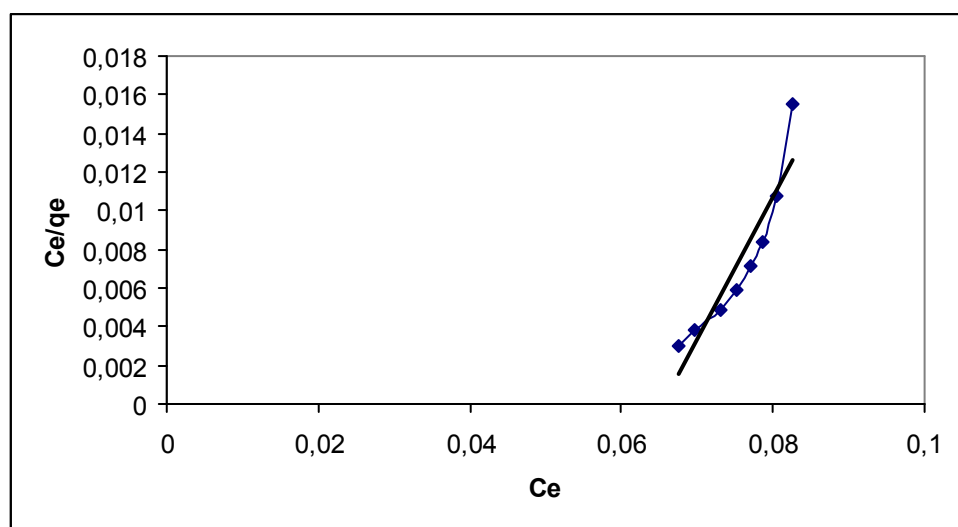


Fig 5. Langmuir sotherm model of 4×10^{-4} M pesticide solution at 25 °C

The Freundlich isotherm equation which corresponds to heterogeneous adsorbent surfaces is given as

$$q_e = K_f \cdot C_e^{1/n}$$

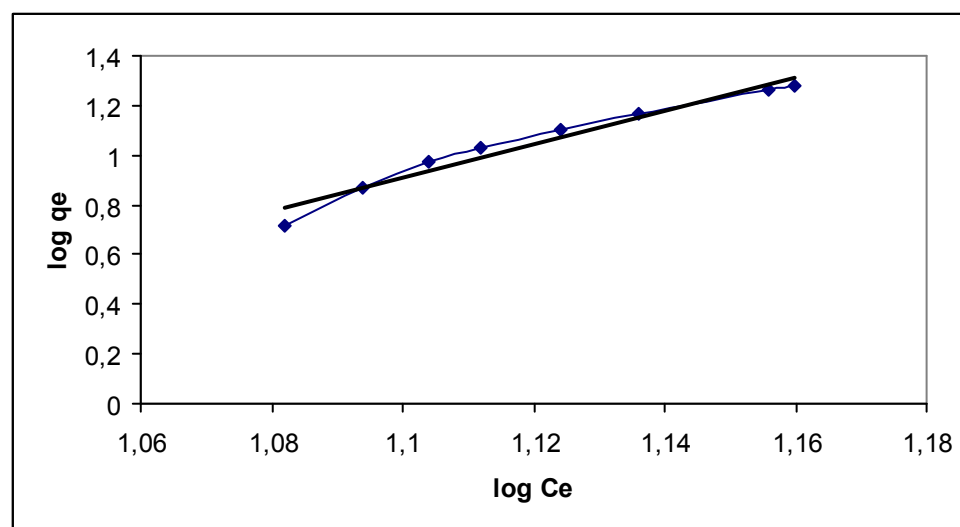
and the logarithmic form is

$$\log q_e = \log K_f + \frac{1}{n} \log C_e$$

where q_e is the amount adsorbed (mg/g), C_e is the equilibrium concentration of the adsorbate (mg/l) and K_f and n are Freundlich constants related to the adsorption capacity and the adsorption intensity, respectively. The values of K_f and n can be calculated from the intercept and slope in Fig 6. The Langmuir and Freundlich constants are given in Table 1.

The Freundlich isotherm gives a better correlation than Langmuir isotherm as is evident from the correlation factors.

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150 Fig 6. Freundlich isotherm model of 4×10^{-4} M pesticide solution at 25 °C

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153 Table 1. The Langmuir and Freundlich constants

Langmuir constants			Freundlich constants		
Q_0	b	R^2	n	K_f	R^2
0.73	-0.049	0.86	0.15	6.46	0.96

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156 3.3 Effect of pH

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158 The pH value of the initial experimental solution was 6. The experiments were performed at
 159 different pH values such as 3, 5, 7, 9 and 11. The pH value of the stock solution was monitored
 160 using either 0.1 N hydrochloric acid or 0.1 N sodium hydroxide solution. The measurements were
 161 performed using WTW series inolab meter.

162 A known weight of adsorbent (0.1 g) was added to each solution. After equilibrium, the
 163 adsorbance equilibrium values were measured by UV spectrometer. The experiments were
 164 performed at temperature of 25 °C. The effect of pH is shown in Figures 7 in terms of % uptake
 165 -pH.

166 Based on experimental values obtained, the adsorption capacity is quite high in acidic medium
 167 (pH=3) at 25 °C as seen from Fig 7. This is due to the acidic character of the pesticide. The

lower adsorption at basic pH is believed to be due to repulsion between the adsorbent surface and pesticide.

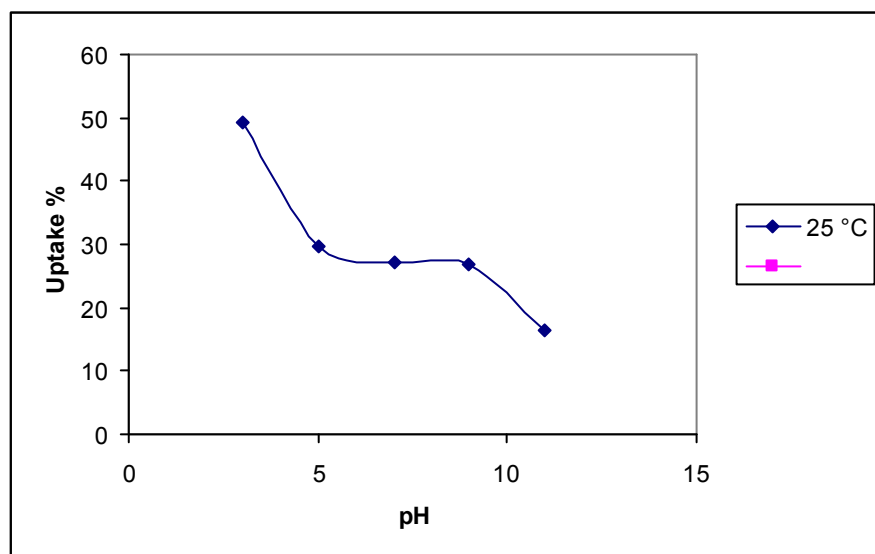


Fig.7 Uptake percent versus pH graphic of 4×10^{-4} M pesticide solution at 25 °C

4. Results

The removal of 2,4-D from aqueous solutions by carbonized chestnut shell has been investigated under different experimental conditions in batch adsorption model. The equilibrium time of adsorption was 4300 minutes for 4×10^{-4} g/l of 2,4-D at room temperature. The batch model adsorption studies were followed with Langmuir and Freundlich adsorption isotherm models. The pH effect was investigated from the point of adsorption yield.

The carbonized chestnut shell was a good and cheap adsorbent which can be utilized in the place of active carbon.

Acknowledgement

This study is supported by the research fund of Yıldız Technical University (YTU BAPK 27-07-01-09)

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